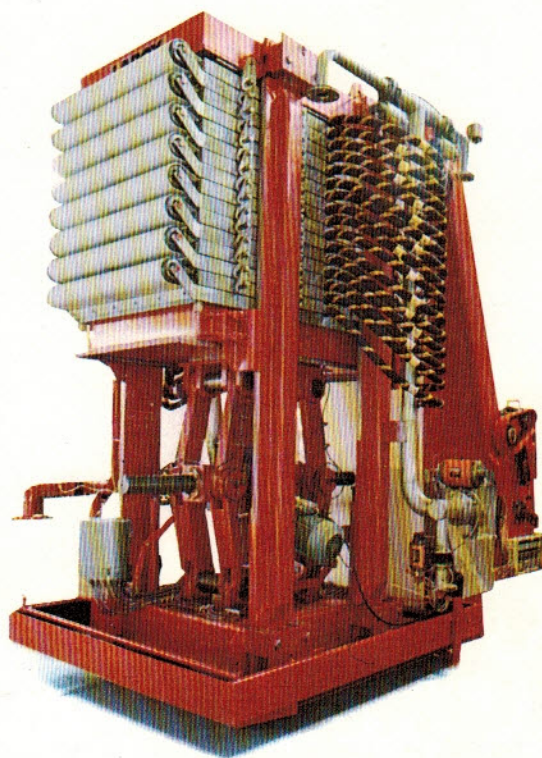


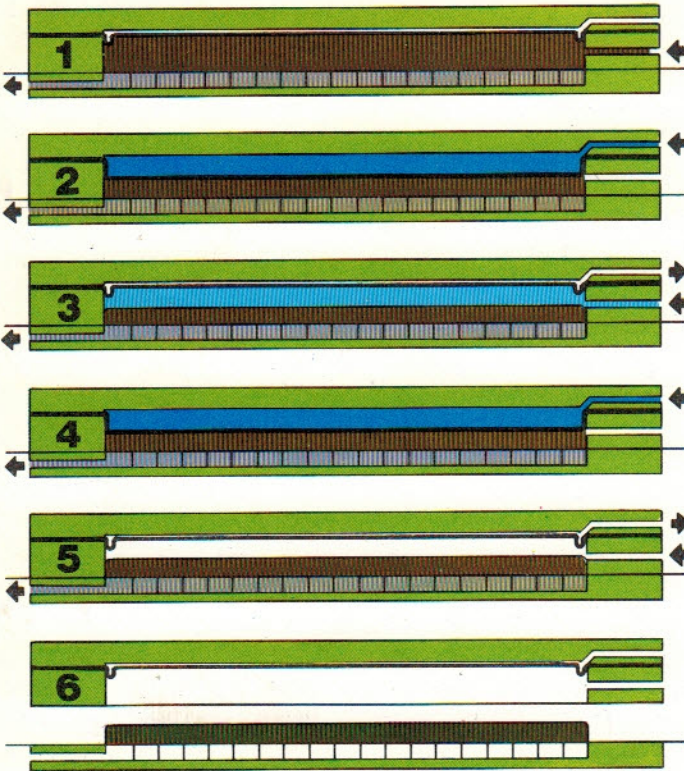
AUTOMATIC PRESSURE FILTER



¹²
11

LAROX

OPERATION



The clamping device presses the horizontal filter units until a pre-set specific sealing pressure is reached.

1 Filtration. The slurry inlet valve opens and the slurry pump starts up. All the chambers are fed simultaneously from the distributing duct and filled in less than one minute.

The liquid phase of the slurry is forced through the filter cloth into the filtrate trough, from which it drains through the vertical discharge duct and a controlled reversing valve to the filtrate flow-off. A timer stops the filtration by closing the slurry inlet valve.

2 Diaphragm pressing I. Pressure water is applied to the diaphragms and the residual moisture is reduced by the compression of the cakes. When the time for compressing the cakes is over, the pressure is released and the pressure water discharge opens.

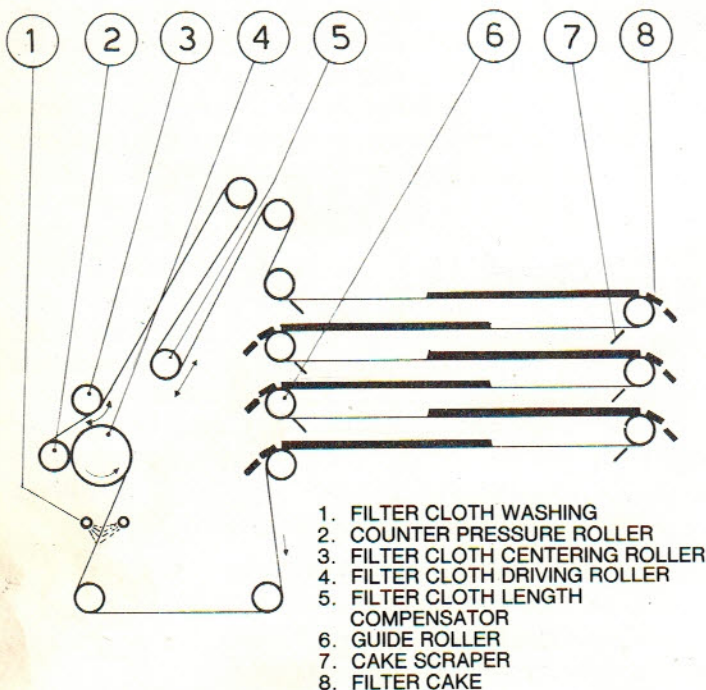
3 Cake washing. The washwater valve now opens and the cake is washed in accordance with the preselected programme.

4 Diaphragm pressing II. After washing, the pressure water valve opens again and the diaphragm presses the cake dry.

5 Cake air blow. To complete the dewatering, the pressure air valve opens and the air flows through the cake. The cake washing, diaphragm pressing and air blowing may be done as often as necessary.

6 Cake discharge. After the cake drying the automatic pressure filter opens. Due to the pick-up links, the clearance between each filter unit is the same.

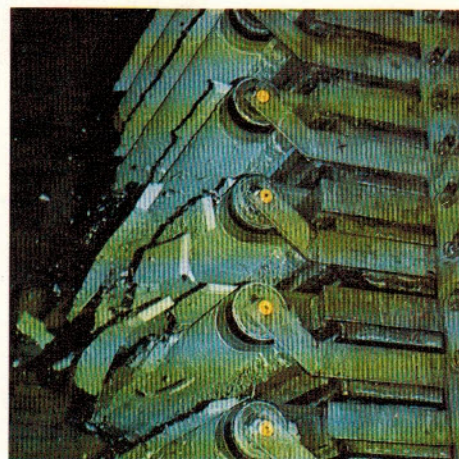
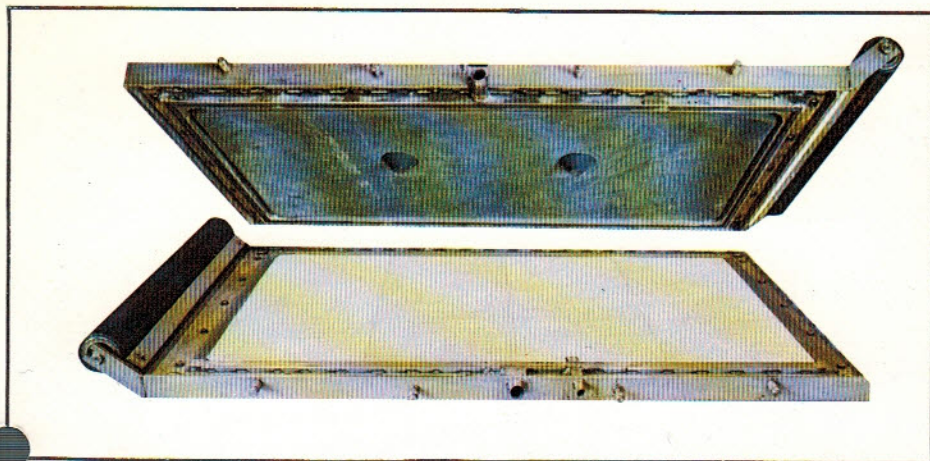
LAROX ¹² **11**



As soon as the pressure filter is open, the filter cloth drive goes into operation. The filter cakes come out from the right and left sides of the machine. As the filter cloth passes the rollers, the cakes disengage from the cloth and broken pieces of convenient size fall down. Pieces of cake remaining on the cloth are scraped off.

The highest purity of filtrate is obtained by installing of additional stationary cloths of finer mesh. The filter cloth washing equipment operates automatically during the run, when the filter cloth is cleaned on both sides by pressure water sprays. After passing the driving rollers, the cleaned cloth is brought to parallel by a centering roller. It enters the filter unit pack after passing the length compensator.

CONSTRUCTIONAL FEATURES



| | | | | | | | | |
|--------------------------------|----------------|---------------|---------------|----------------|----------------|----------------|----------------|----------------|
| Type: PF | | 2,5 | 5,0 | 9,5 | 12,5 | 19,0 | 25,0 | 32,0 |
| Filter area | m ² | 2,5 | 5,0 | 9,5 | 12,5 | 19,0 | 25,0 | 31,5 |
| Interplate clearance | mm | 45 | 45 | 45 | 45 | 45 | 45 | 45 |
| Max operating pressure | bar | 16 | 16 | 16 | 16 | 16 | 16 | 16 |
| Number of filter plates | | 6 | 12 | 6 | 8 | 12 | 16 | 20 |
| Filter cloth dimensions | mm | 650× 16500 | 650× 26500 | 1050× 25000 | 1050× 30000 | 1050× 40000 | 1050× 46500 | 1050× 53000 |
| Installed power | | | | | | | | |
| — Clamping mechanism | kW | 3 | 3 | 7,5 | 7,5 | 7,5 | 7,5 | 7,5 |
| — Cloth tensioning device | kW | 0,75 | 0,75 | 1,1 | 1,1 | 1,1 | 1,1 | 1,1 |
| — Cloth moving mechanism | kW | 1,5 | 1,5 | 4 | 4 | 4 | 4 | 4 |
| — Water pump | kW | 4 | 4 | 7,5 | 7,5 | 7,5 | 7,5 | 7,5 |
| Overall dimensions | | | | | | | | |
| — length | mm | 2550 | 2850 | 4000 | 4000 | 4000 | 4000 | 4000 |
| — width | mm | 1300 | 1300 | 2000 | 2000 | 2000 | 2000 | 2000 |
| — height | mm | 2350 | 3065 | 2565 | 2800 | 3275 | 3750 | 4350 |
| Total floor space requirements | m ² | 16 | 16 | 30 | 30 | 30 | 30 | 30 |
| Weight, tons | | | | | | | | |
| — filter proper | t | 4,8 | 6,5 | 10,3 | 11,1 | 12,6 | 14,0 | 15,7 |
| — filter with auxiliaries | t | 6,3 | 8,0 | 12,6 | 13,4 | 14,9 | 16,3 | 18,0 |

A single filter unit, forming a filter chamber, consists of the plate, frame, collector sections, diaphragm, supporting grid and perforated sheet.

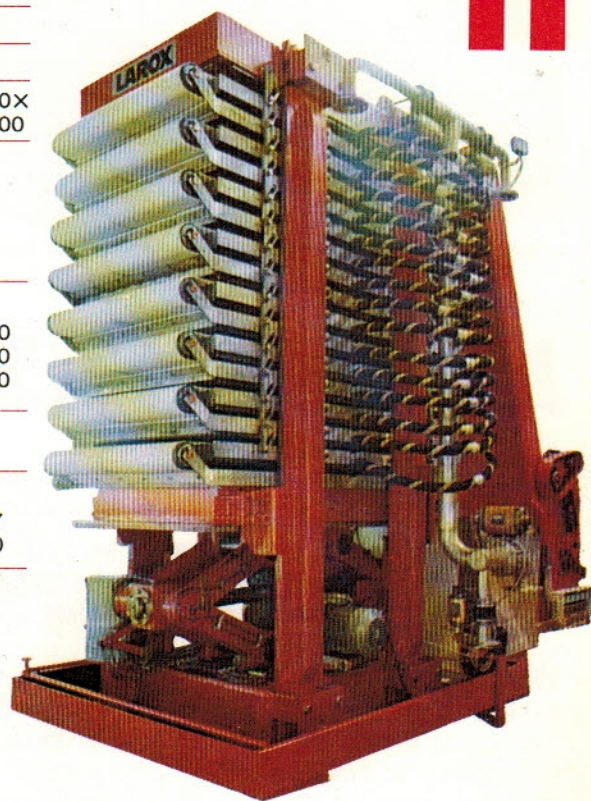
A diaphragm fixed in the frame and lies on the rough. Pressure can be applied to the back of the diaphragm, when the bottom of the diaphragm forms the top and sides of the cake chamber. Each filter unit has a common connection for slurry, wash liquid and drying air, and a second piece of the same shape for filtrate discharge.

The filter cloth zigzags through the pack of filter units and after leaving the lowest enters a washing vat. The cloth is thoroughly cleaned in the washing vat by pressure liquid from spraynozzles.

A regulating roller is followed by a cloth length compensator covering approx. 10 % of the length.

The pressure medium, preferably water, is brought from a distributing pipe to the back of the diaphragm of each filter unit by means of connecting hoses.

The pressure filter is a fully automatic machine. It can also be run semi-automatically, i.e. after starting the closed machine the individual operations: "Filtration", "Compression I", "Washing", "Compression II",



"Drying", and "Discharge" are initiated by pressing the relevant push-button. Each operation stops on pressing the push-button for the next operation or for the full stop. It is possible to exclude one or more operations in the above-mentioned sequence.

The filter is made in three standard executions:

1. **Stainless steel construction for non-corrosive applications,**
2. **stainless steel construction for corrosive applications and**
3. **acid proof construction for extra heavy corrosive applications.**

ADVANTAGES

The Larox Automatic Pressure Filter increases output some four to ten fold in comparison with the plate-and-frame presses, sharply cuts expenditure on filter cloth and makes the process of filtration fully automatic. One operator can run up to ten pressure filters.

- greater filtering area for a relatively small floor space;
- filtration and cake drying at a pressure of up to 15 bars at optimum cake thickness;
- filter cakes are dried by hydraulic pressure exerted over rubber diaphragms, thus considerably saving the compressed air required for drying;
- auxiliary operations take little time (filter opening, cake discharge, and closing take 1—5 minutes altogether);
- efficient cleaning of filter cloth in the course of operation;
- efficient cleaning of filter cloth in the course of operation;
- efficient and economical wash of filter cakes, due to the diaphragm assembly and horizontal position of the plates;
- fully automatic operation, allowing rapid adjustment of the filter for the maximum efficiency of the process;
- automatic discharge of filter cakes;
- weight of filter, in relation to the weight of filtered product, is 2—3 times less than in the present plate-and-frame presses.

PERFORMANCE DATA

The automatic pressure filter is already running successfully in a large number of industries, e.g. the ceramics, foodstuffs, dyestuff, chemical and mining industries, as well as in steel works and waste water treatment plants.

The table lists the operational results achieved in these applications. The average values of operational filtration data obtained with the automatic pressure filter are compared with those obtained with

other filtration equipment. If washing operations are necessary, they considerably affect the specific filter performance and the filtering area required. This means increased operational expenditure which, however, is at its lowest in the case of the automatic pressure filter because of the reduced washing time and better washing efficiency.

All data are applicable only under the same operating conditions as when they were obtained.

| Field of application Product and process | LAROX-PF | | OTHER FILTRATION EQUIPMENT | | |
|---|--|-----------------------------------|----------------------------|---|-----------------------------------|
| | Capacity dry cake kg/m ² h | Residual moisture % in cake | Filter type | Capacity dry cake kg/m ² h | Residual moisture % in cake |
| Ceramics | | | | | |
| Kaolin | 36—40 | 28—30 | Chamber filter press | 7—8 | 33—34 |
| Talc | 200—700 | 10—15 | Plate and frame filter | 8—12 | 20—22 |
| Mining Industry | | | | | |
| Coal Sludges | 80 | 20 | „ | 8—9 | 22—24 |
| Oil Industry | | | | | |
| Crude Oil | 1,3—1,5 | 62 | „ | 0,15 | 78 |
| Dye-Stuff Industry | | | | | |
| Acid Orange | 10—13 | 47—50 | „ | 0,685 | 52—54 |
| Light-Fast Substantive Bordeaux | 5—7 | 64—66 | „ | 0,7 | 70—72 |
| Bright Green Neutral | 1,7 | 76 | „ | 0,17 | 80 |
| Bright Green Acid | 1 | 78 | „ | 0,24 | 80 |
| Golden Yellow | 7 | 65 | „ | 0,33 | 70—74 |
| Dioxylacton | 5,5 | 42 | „ | 0,25 | 50—60 |
| Bright Orange | 17,2 | 62 | „ | 0,25 | 85 |
| Light-Fast Acid Scarlet | 1,7—2 | 50—52 | „ | 0,3 | 59 |
| Food Industry | | | | | |
| Sugar Industry Juice | 65—75 | 40—43 | Vacuum drum filter | 35—40 | 50—51 |
| Hydro-Metallurgy | | | | | |
| Tungstic acid production | | | | | |
| first leaching | 100 | 4—8 | „ | 10 | 20—21 |
| second leaching | 60—70 | 13—15 | „ | 6—7 | 25—30 |
| Lime Suspension | 120 | 44—46 | „ | 15 | 55—60 |
| Magnesium Fluoride | 50 | 35—37 | „ | 9—10 | 42—45 |
| Gel, Polysilicic acids | 3—18 | 45—55 | „ | 0,7—3 | 60—65 |
| Molybdenum Trisulphide | 5 | 55—60 | „ | 1,6—1,7 | 65—70 |
| Zirconium Sulphate Solution | 50—54 | 20—25 | — | | |
| Copper Cadmium Sludge | 5—6 1,0—1,2 m ³ /m ² h | | Plate and frame filter | 1,0—1,1 0,15—0,8 m ³ /m ² h | — |
| Zinc Oxide | 45 | 41 | „ | 6—8 | 50 |
| Zinc Stearate | 110 | 25—28 | Centrifuge | 50 | 34—35 |

| Field of application Product and process | LAROX-PF | | OTHER FILTRATION EQUIPMENT | | |
|--|---|-----------------------------------|----------------------------|--|-----------------------------------|
| | Capacity dry cake kg/m ² h | Residual moisture % in cake | Filter type Filter type | Capacity dry cake kg/m ² h | Residual moisture % in cake |
| Rare-Metals Separation in Zinc Production | | | | | |
| Arsenic Refining Solutions | 65—70 | 40 | — | | |
| Solution for Selenic Cake Leaching | 28—30 | 25—28 | Plate and frame filter | 8—10 | 30—35 |
| Solutions for Sulphate Product Leaching | 115—120 | 15 | Vacuum Disc filter | 16—18 | 26 |
| Solution for Copper- Chlorine Cake Leaching | 55—58 | 35 | Plate and frame | 4—5 | 40—45 |
| Dust Catching Solution | 25—30 | 25 | Vacuum Disc filter | 9—10 | 35 |
| Calcium Arsenite Suspension | 110—115 | 45 | „ | 10—11 | 50 |
| Solution for Washing Selenium-Arsenic Cakes | 25—30 | 43 | „ | 1,5—2 | 50 |
| Aluminium Production | | | | | |
| Red Slurry from Washing Clarifiers | 55—60 | 20—25 | Kelly filters | 15—18 | 45—50 |
| Bariumsalt Production | | | | | |
| Water Leaching | 70 0,6 m ³ /m ² h filtrate | 30—35 | Plate and frame filter | 5—6 0,04—0,05 m ³ /m ² h filtrate | 45—47 |
| Acid Leaching | 7—18 0,15 m ³ /m ² h filtrate | 60 | Plate and frame filter | 3—4 0,03—0,035 m ³ /m ² h filtrate | 65—70 |
| Ferrous Metallurgy | | | | | |
| Silico Manganese | 68 | 35 | — | — | 500—600 g/l concentration |
| Blast Furnaces | 110—140 | 25—29 | Sedimentation | — | 500—600 g/l concentration |
| Siemens-Martin Steel Furnaces | 25—30 | 18—20 | Sedimentation | — | 250—300 g/l concentration |
| Ferro-Alloy Furnaces | 25—30 | 40—42 | Sedimentation | — | 90—120 g/l concentration |
| Neutralized Etching Effluent | 3—4 0,24—0,32 m ³ /m ² h filtrate | 65—70 | Sedimentation | — | 12—15 g/l concentration |
| Fluorine Production | | | | | |
| Sodium Bifluoride | 80—95 | 14—16 | Centrifuges | 40—50 kg/h | 12—15 |
| Synthetic Rubber | | | | | |
| Catalyst Masses | 0,55 double slurried | 69—70 | Plate and frame | 0,11 double slurried | 72—75 |
| Silica Gel Production | | | | | |
| Rubber Filling Material | 6—8 | 67—72 | Vacuum drum | 4 triple slurried | 79—82 |
| Catalyst Carrier | 4 | 75—77 | — | — | — |
| Ammonia | 8—9 | 68—70 | Belt filter | 3—4 triple slurried | 85 |
| Municipal Sewage | | | | | |
| Sludge | 14—17 | 42—56 | Plate and frame filter | 6—9 | 55—65 |

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